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Micropolar Fluids Properties and Applications in Engineering and Science

Prathap Kumar, JawaliChannabasappaUmavathi and Appasaheb Sharanappa Dhone

*Department of Mathematics, Gulbarga University, Karnataka, India

Abstract: This paper presents an analysis of micropolar fluid past a wedge, considering the effects of viscous dissipation and heat absorption for flow systems doped with gyrotactic microorganisms. The transport model developed using nonlinear PDEs was transformed into a set of equivalent ODEs through suitable transformation equations. The shooting technique in micropolar fluid, in conjunction with the Runge-Kutta-Fehlberg integration scheme in microorganisms, was used to solve the obtained set of equations numerically. The effects of key factors on non-dimensional momentum profiles, temperature, and motile bioconvective Lewis microorganism density were estimated for the impact of pressure gradient parameter, Eckert number, material parameter, heat sink, and bioconvection Lewis number. The numerical data obtained was graphically presented, and the consequences of the major factors were thoroughly described in both the cases of Blasius and stagnation flow. Micropolar fluid is a type of fluid that displays microscopic impacts due to the phenomenon of fluid particle micromotion. The effectiveness of liquid crystals, lubricants, animal blood flowing through rigid cells, and other substances can be discussed using micropolar fluids. The unique feature of this fluid class is couple stress sustenance. This study is important for understanding the behaviour of micropolar fluids and can be applied in various fields, such as lubricants, cooling of metal plates in a bath tub, animal's blood, and physiological fluids, among other things. The numerical data obtained in this study provides new insights into the behaviour of micropolar fluids and can serve as a basis for further research in this field. Overall, this study provides valuable insights into the properties and applications of micropolar fluids in engineering and science.

Keywords: micropolar fluids, non-Newtonian fluids, rheological models, couple stress sustenance, thermal energy, heat transfer, engineering, science.

1. INTRODUCTION

The viscosity law of Newton does not apply to non-Newtonian fluids. Because of industrial and engineering goals, the importance of non-Newtonian fluids has garnered a lot of attention in current years. Chemical reactions and lubricants, bioengineering materials, material fabrication, polymer mixes, and other applications necessitate the use of such fluids. Molten polymers, paints, scrub, blood, unguent, maquillage, and foods such as ketchup, cheese, honey, soups, taffy etc. are examples of non-Newtonian fluids, as are natural resources like petroleum, lava, and some kinds of dispersions. Food digesting, antibiotic dispensing, and biomedical sectors such as toxin elimination and cancer therapy may all have important responsibilities to consider. Because of the inclusion of rheological influences in their constituent regulating equations, non-Newtonian liquids and their dynamic properties have a lot of complications. Over the past 20 years,

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researchers' interest in the thermo-physical characteristics of these fluids has increased [1, 2]. In several disciplines of chemical and material processing engineering, non-Newtonian transport phenomenon occurs. Compared to the Newtonian (Navier-Stokes (N-S)) model, shear-stress-strain correlations in such fluids deviate greatly. In almost all non Newtonian models, the momentum conservation equations are altered in some way. Power-law, thixo-tropic, and visco-elastic fluids are among them [3]. However, microstructural features of many critical liquids, such as polymer suspensions, physiological fluids, contaminated lubricants, and so on, are impossible to simulate using such rheological models. Micropolar liquids are the name given to these types of liquids [4].

Micropolar fluid is a type of fluid that displays microscopic impacts due to the phenomenon of fluid particle micromotion. This fluid is made up of stiff macromolecules that move independently and maintain stress and body moment through spin inertia. The effectiveness of liquid crystals, lubricants, animal blood flowing through rigid cells, and other substances can be discussed using micropolar fluids [5]. These fluids are composed of randomly arranged particles dispersed in a sticky medium that can rotate and alter the flow's hydrodynamics, making them nonNewtonian fluids [6]. A unique feature of this fluid class is couple stress sustenance. Eringen [7] proposed the micropolar material model for microstructural fluids to overcome these challenges. Two new velocity variables are introduced in the micropolar fluid theories that were not included in the N-S model. These microrotational parameters reflect the spin and microinertia tensors that describe the distributions of atoms and molecules inside minute fluid particles. Following that, a number of researchers looked at the micropolar liquid from various angles [8-14]. It is used to investigate the behaviour of novel lubricants, liquid crystal solidification, and extraction of polymer fluid, cooling of metal plates in a bath tub, animal's blood, and physiological fluids, among other things [15]. Eringen [16] went on to expand on the micropolar fluid idea and coined the term "thermomicropolar fluids". The implication of chemical reactions on the flow of a micropolar nanofluid via a wedge was inspected by Zulkifli et al. [17]. The impact of chemical processes on the thermal energy and mass transport flows of a magneto-micropolar fluid through a non-conducting wedge containing Hall and Ion-slip currents was inspected by Singh et al. [18]. The Soret and Dufour influences on the heat transport processes of micropolar fluids on a thick needle travelling in a parallel flow were numerically explored by Maboob et al. [19]. Falkner and Skan [20] explored the issue of boundary-layer flow on a wedge for the first time, introducing suitable transforms identified as Falkner-Skan solutions that may be used to fluids with like flows to convert differential boundary-layer equations to ODEs. After that, Hartree [21] examined the Falkner-Skan flow problem quantitatively. The concept of non Newtonian (micropolar) fluid flow around the wedge, as addressed in the paper, is undoubtedly a fascinating issue to consider because the fluid might refer to a variety of fluid types with complex properties that are not explained by Newtonian fluid. Many sectors of engineering and science use heat exchange and boundary layer flow across a wedge-shaped body. Elbashbeshy et al. [22] researched the heat exchange flow on the wedge surface. Xenos et al. [23] evaluated the influence of turbulent flow on a wedge surface. For a range of physical processes, several writers [24–30] explored fluid flow and heat movement in surface wedges.

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In many physical models, heat transport through a heat source/sink is the most notable element. When there is a considerable thermal energy variation between the surrounding fluid and the surface, the influence of heat creation (source) or absorption (sink) seems to be quite substantial. The heat source, which is often dependent on temperature and space, has a noticeable impact on the fluid's heat transmission capabilities. Controlling heat transfer is greatly influenced by the heat source/sink. Tufail et al. [31] employed Lie group analysis to find similarity results for non Newtonian flow with a magnetic-intensity and a heat source or sink involving a magnetic intensity. The flow of non-Newtonian nanofluids with magnetic flux and a heat sink/source was studied by Ramesh et al. [32]. Pal [33] looked into how fluid flow, which is dependent on time, on a strained surface including an uneven heat sink or source affected thermal transfer. Kumar et al. [34] examined the heat exchange properties of ferrofluid flow across a convective sheet containing radiation. Mabood et al. [35] researched the impact of a changing heat source and sink on the flow of micropolar fluid over a stretched sheet including thermo-diffusion. Makinde et al.[36] and Mabood et al. [37] investigated the effects of heat source or sink, and radiation on the nanofluid flow over a non-linear surface and came to the conclusion that the heat sink factor tends to raise temperatures. The fully formed thermal energy and mass transport of a micropolar liquid through a upright channel including a heat source and sink is explored by Umavathi et al. [38]. Many scholars, such as [39–45], have looked into the significance of non-uniform heat sink or source affects in many forms of flows.

Microorganisms like bacteria and microalgae are heavier than water and so have the ability to travel in the reverse direction of gravity. The density of the topmost layer of suspension gets so large as a result of the conglomeration of microorganisms that the density distribution in the suspension's bottom layer becomes unstable. Hence, convective instability develops, and convection patterns begin to form. Bioconvection is the term for the voluntary and random movement of microorganisms. Many researchers have studied this phenomenon because of its practical uses in commercial, industrial, and environmental items such as ethanol, fertilisers, and fuels. Bioconvection is a macroscopic convective motion caused by the correlated movement of motile microorganisms in fluid. Because microorganisms are denser than fluid, their movement causes a rise in fluid density. This happens because of upward self-derived motion, which causes a stratified layer to emerge on the upper portion of the fluid. The combined convected micropolar nanofluid flow with magnetic flux, energy of activation, and gyrotactic microorganisms is described by Waqas et al. [46]. As per the existing/available literature, the improved micropolar fluid including gyrotactic microorganisms has received less attention than the critical engineering and industrial applications. Kuznetsov et al. [47-48] have visualised several recent achievements in this field.

The bioconvective Carreau nanofluid flow with a magnetic effect on thermal radiation and velocity slip is studied by Muhammad et al. [49]. The outcomes of several fluid models, such as Newtonian, micropolar, Williamson, and Maxwell, for mass and heat transfer due to expanding surfaces, including microorganisms, are compared by Habib et al. [50]. Song et al.[51] investigated the bioconvection flow of the Brinkman form of micropolar fluid related to an extending inclined surface when there was liquefying thermal performance. Khan et al.[52] have studied magnetised micropolar fluid flows, including motile microorganisms with changeable heat conductivity travelling across a moving surface. Abiconvection study of micropolar fluid



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flow containing microorganisms with activation energy was studied by Abdelmalek et al. [53]. The flow of 2-D Casson nanofluid across a wedge having swimming and motile microorganisms with heat and activation emission has been examined by Waqas et al. [54].

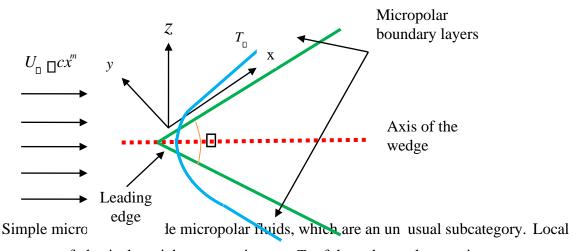
The true purpose of this topic, which is motivated by the above literature, is to investigate biconvective micropolar fluid flow with heat source/sink and material properties over a wedge. In the fluid modelling, the Eckert number and the FalknerSkan parameter are taken into account. Based on the above literature assessment, it appears that the impact of gyrotactic microorganisms on micropolar fluid flow receives less attention. Several essential features have shown a negligible effect on secondary velocity. Nanotechnology, biotechnology, food industries, cancer therapy, polymer coating systems and a wide range of other industries etc. can all benefit from the existing approach.

1.Problem formulation

We take into account the 2-D forced convective fluid flow over a wedge that is incompressible, steady, and contains motile microorganisms. The authors utilize rectangular coordinates $(x \ y \ z, \ ,)$, where x, y, and z correspond to measurements along the wedge, normal to the topside of the wedge, and in the direction of wedge's main edge, respectively. The wedge lies in the $xy \square plane$, where the fluid flow is in the direction of the x-axis. As shown in Fig. 1, the wedge is positioned so that its surface lines up with the x-axis and the y-axis is vertical to it. The $xy \square$ plane is perpendicular to the z-axis. Fluid flow is thought to be created by extending a wedge at a velocity of U in the current investigation. Assume the exterior velocity of the wedge is $U \times cx() \square^m$, here c- is the positive constant, $m \square \square^m / 2\square \square^m$, wedge parameter with $0 \square m / 1$,

 \square \square * \square \square / . The flow is decelerated (retardation) for \square * \square 0, whereas it accelerates for \square * \square 0, and \square * \square 0 correspond horizontal flat plate to fluid flow. To make the problem easier to understand, the authors assume that the flow and heat transport amounts in the z $\square axis$ do not change.

Axisymmetric



movements of physical particles present in every T_w of the volume element, i.e.

Figure 1. Physical model

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Mass conservation

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microelement, influence the behaviour and properties of these fluids, and thus have local inertia. Volume elements in micropolar fluids comprise hard (non-deformable) particles that can spin around the volume element's centre and are described by a microrotation vector. The customary stiff body movement of the full volume element, that describes N-S fluids, is supplemented with this local movement of the particles. Thus, supplementary equations that consider the conservation of micro-inertia moments and the balancing of initial stress moments, both of which emerge as a result of the study of microstructure in a fluid, are added to the classical continuum laws in the mechanics of micropolar fluid. As a result, classical (continuity of) fluid dynamics theory is combined with novel kinematic variables, as well as ideas of stress moments, and microstress. For micropolar fluids, the field equations in vector form are as follows [7, 56]:

$\underline{\hspace{1cm}}t \square \square \cdot \square \square^{V} \square \overline{\hspace{1cm}}0 (1)$			
Translational momentum conservation			
$\begin{smallmatrix} & & & & & & \\ & & & & & \\ & & & & & \\ & & & & \\ & & & & \\ & & & & \\ & & & \\ & & & \\ & & & \\ & & & \\ & & & \\ & & & \\ & & & \\ & & $		$\square V \square \square \square \square$	$V \square G P$
$\Box \Box f \Box V^{\Box}$ (2)			
Rotational momentum (micro-rotation) conservation			
$ \begin{smallmatrix} & & & & & & & \\ & & & & & & \\ & & & &$	$G \square V2 \square \square \square$	$\exists G \Box \ \Box l \ jG^{\boxminus}$	(3)
The velocity (known from the N-S hypothesis) and the axial v	ector field, wl	nich mimics th	e spin of the
micropolar fluid molecules, are the only two distinct kinematical	vector fields th	nat we are conc	erned with in
the theory of the micropolar models. These are supposed to be ri	igid. We shoul	d remark that	in micropolar
fluid theory, there are no external body forces in which the fluid	has fixed phy	sical characteri	istics, and the
conservation equations for steady state flow are considerably redu	uced. Furtherm	nore, when \Box	
$\ \square$ 0 and lf are vanishing, the gyration vector vanishes, and	eqn. (3) disa	ppears comple	etely. In this
exceptional instance, equation (2) also simplifies to the tradition	al N-S Eqs. T	he momentum	vector V and
the microrotation G are uncoupled when $K \square 0$ only, and the	global move	ment is not af	fected by the
microrotations. For the axisymmetric wedge problem with a fixed	ed thermal flux	on the wedge	e surface, this
model was used. The ambient fluid's temperature (T_{\square}) (free stream	m) is considere	ed to be stable.	The equation
for the micropolar fluid system including motile bacteria is: Cont	inuity,	_	
$ \qquad \qquad \Box^u \Box^{\Box v} \Box 0 (4)$			
$\Box x \Box y$			
Linear (translational) momentum conservation along $x \square$ axis:			
$\square \ \square u \ \square u \ \square \qquad \square^2 u \ \square N \ dU$			
$\overline{u}_{x} \cup v_{y} \cup \overline{u}_{x} \cup v_{y} \cup \overline{u}_{y} \cup \overline{u}_{y} \cup \overline{u}_{y} \cup \overline{u}_{y} \cup \overline{u}_{y}$	U = dx (5)		
Linear (translational) momentum conservation along $z\square$ axis			
$\square \square w \square w \square \square^2 w$			
$ u_x v_y v_y v_y v_y v_y v_y v_y v_y v_y v_y$	2 (6)		

Angular momentum (microrotaion) conservation
Energy conservation
$\square \ \square T \square T \ \square \square \square^2 T \ \square \qquad \qquad \square \square u \square^2 \ \square \square w \square^{2\square}$
$\square C up \square x \square \overline{v} \square y \square \square \square \square \square \square \square y 2 \square \square \square \square \square \square \square \square \square$
Density of gyrotactic microorganism
$u^{\square M} x \square v^{\square M} y \square D_m \square_{x}^{M_2} \square \square_{y}^{2M_2} \square \square_{x}^{2M_2} \square_{x}^{2M_2} \square \square_{x}^{2M_2} \square_{x}^{2M$
Where $\Box \Box j$. The relevant boundary constraints are given on the wedge surface and at the
boundary layer regimes border on the stream (far off the wedge).
They are of the following kind:
$u \square 0, v \square 0, w \square 0, N \square \square n \underline{\hspace{1cm}}^{\square u}, q_w \square \square k \underline{\hspace{1cm}}^{\square T}, M M \square w \text{ when } y \square 0 $ (10a)
$\Box y \qquad \Box y$
$u \square \square U \qquad cx^m; w \square 0, N \square 0, T \square T_\square, M \square M_\square \text{as } y \square \square $ (10b)
The parameter m in equation (10b) has multiple significant values that correspond to traditional flow
configurations. There are four situations worth mentioning:
Case 1: When \square^* is in the interval(0,2), this means $m\square$ 0, the flow is a generalised 2-D wedge flow.
Case 2: When $\square^* \square 0$, for which $m \square 0$, on a horizontal, flat plate that is partially infinite, fluid flows.
Case 3: Forward stagnation point flow close to the upright surface happens when $\Box^* \Box 1$ implies $m \Box 1$.
Case 4: Rear stagnation-point flow close to the vertical surface happens when $\square^* \square \square 1$ that implies $m \square \square 1/3$.
The starting three scenarios are the most essential to polymeric coatings. When it comes to heat transport,
these scenarios are also completely valid. The micro-rotation border restrictions, which are governed by the
value of n in (10a), permit for a wide range of physical possibilities to be investigated. In this scenario, we
will use $n \square 0.5$, that relates to a low micro-element concentration near the wall. The situations $n \square 0$ and
$n\square$ 1 are linked with significant at the wall concentration and turbulent flows, respectively, but none of these
are pertinent in our study. As a result, the micropolar fluid model includes a separate angular momentum
balance together with additional boundary requirements/constraints. Considering Equations (5) and (7)
implies a strong connection amidst the angular momentum and primary translational momentum profiles,
despite the absence of partial derivatives, as in previous visco-elastic model's. Solving the parabolic PDE's
(4)–(9) remains a difficult task. Consequently, the boundary value issue can be transformed to produce more
numerically tractable solutions. As a result, we establish the scaling transformations and non-dimensional variables below as well as a stream function \Box given by $u = \Box$ and $v = \Box$ that effortlessly follows
variables below, as well as a stream function \square , given by $u_{\square} = \square^{\square}$ and $v_{\square} = \square^{\square}$, that effortlessly follows
mass
$\sqcup y \qquad \qquad \sqcup x$

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conservation:
$\square \square \square \square \overline{m} \square 1 \square \overline{U} \square \square 1/2 \qquad \square 2 \overline{\square x U} \square 1/2 F() \square , \qquad w \square UG \square \square ,$
$y , \Box \Box \Box$
\square $2\square x$ \square $m\square 1$ \square
$\square \square m \square 1 \square U \square^{1/2} \qquad \qquad k \ T \ T \square \square \square \square m \square 1 \square U \square^{1/2}$
NUH
\square $2\square x$ \square qw \square $2\square x$ \square
2xQx()
$\square \square \longrightarrow , K \square \qquad \qquad \underbrace{- ,}_{i \longrightarrow U^2} \qquad I \square (11)$
$\overline{U^2}$
$\Box C U_p$ \Box j $\overline{}$
$C_p \ \Box T \ \Box T_\Box \ \Box$
Utilizing equations (11), the Eqs. (4–8) are simplified to the coupled set of nonlinear equations that are listed
below:
Primary momentum
$\square 1 \square KF \square ""\square KH "\square FF" \square \square $
Secondary momentum
$\square 1 \square KG \square "\square \square \square $
Angular momentum
$m2KI \square 1 \square \square \square F \square 2H \square \square 0 (14) \square$
Energy,
$ \square \square $
$\square \square \square \square \square m \ 1 \square F \square' \square \ 0 \ (15)$ Density,
2
$2\sqrt{\frac{m}{2}}$ $m = 1$
$lackbox{V}$ $lackbox{2}$
$\square \square 4 \square m \square 1 \square \qquad \sqrt{\frac{m \square 1}{2}} \qquad \text{Re } \square 2 Lb \text{Re} \square m \square 1 \square F \square \square$
The relevant converted boundary restrictions are ascertained as:
$F(0) \square 0$, $F'(0) \square 0$, $G(0) \square 0$, $H(0) \square \square nF''(0)$,
$\Box'(0) \Box \Box 1, \Box(0) \Box 1$ at $\Box \Box \Box 0$
$F'(\square \square)1, G(\square \square)0, H(\square \square)0, \square(\square \square)0, \square(\square \square)0$ as $\square\square\square$ (17)

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2. Physical quantities

We are keen in the momentum, micro-rotation, temperature, and density of microorganisms in engineering computations, as are a few of their gradient functions.

The primary and secondary dimensional wall shear stresses are expressed in the form:

The primary friction drag is as follows:
$2\Box x$
$Cfx \square U2 \square$
The secondary friction drag is as follows:
$2\square wCfz \square U2 \square$
The following formula is used to determine the wall couple stress:
$Cw \square \ cwU^\square 32$ ——
The dimensional Nusselt number is calculated as follows:
xqw
$N_u \square k T \square \square T_{\square} \square$
The dimensional local microorganisms number can be calculated as follows:
xqn
$\operatorname{Mn} \Box D_m \Box M_w \Box M_\Box \Box$
Where $\Box x \Box = U2 \ 2 \ \Box \Box \Box \Box = \Box \Box uy \Box N \Box \Box y \Box 0$, $\Box \Box w$
$\square \square \square \square \square \square wy \square \square y \square 0,$
$c_w\square_{\square}^{\square N}$ $ _{y\square 0}$ — $q_w\square_{\square}k^{\square T} _y$ — $q_w\square_{\square}k^{\square T} _y$ — $q_w\square_{\square}D_m^{\square M} _{y\square 0}$ and Re
The following are the physical quantities in dimensionless form:
$C_{fx}\operatorname{Re}^{1/2}\Box 2(m\Box 1)^{\Box}\Box 1\Box^{K}{}_{2}\Box^{\Box}F''(0),$ $C_{fz}\operatorname{Re}^{1/2}\Box 2(m\Box \sqrt{)}\Box 1\Box KG\Box'(0), C_{w}\operatorname{Re}$ $\Box C_{fx} \Box C_$
$C_{fz} \operatorname{Re}^{1/2} \square \ 2(m\square) \ \square \ 1\square K \ G\square \ (0), C_w \operatorname{Re} \qquad \qquad \square $
$Nu \operatorname{Re} \square 1/2 \square \sqrt{\frac{m \square 1}{2 \square (0)}} \operatorname{Re} \square 1/2 \sqrt{\frac{m \square 1}{2}} \qquad \square \square \square'(0) $ (18)
$\sqrt{2} \square (0)$ $\sqrt{\frac{1}{2}}$
It is worth noting that the gradients $F''(0)$, $G''(0)$, and $H'(0)$ can be used to investigate
skin frictions, wall couple stress, heat exchange rate, and local microorganisms number. The current flow
model has a number of pertinent special situations. Newtonian convection is described by the flow model as
$K \square 0$. Viscous heating is prohibited when $Ec \square 0$ and there is no heat sink when $\square \square 0$.When $m \square 0$, the
flow on the wedge transforms into Blasius flow through a flat plate. When $m \square 1$, the example of flow near a
stagnation point on an unending plate is recalled.

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3.Results and Discussion

Sixesures and Discussion
An extensive number of computations are carried out with different parameter values to understand the
nature of primary velocity, angular velocity, temperature and motile microorganisms and are displayed in
Figures 2 – 6. The default parameters chosen are $I \square 0.5$, $K \square 0.5$, $m \square 1/3$, $Pr \square 100$, $\square \square \square 0.5$, $Ec \square 0.2$ and
$Lb\Box 1.0$.
Figs. 2a – d explain the impact of pressure gradient factor (m) on $f'(\Box)$, $H(\Box)$, $\Box\Box($) and $\Box\Box($)
respectively. As stated before, for $m \square 0$, Case-II acquired, i.e., flow through a semi-infinite horizontal plane
also called Blasius flow. When mis equal to one, Case-III is retrieved, i.e., forward stagnation-point flow
$(\Box \Box 180^{\circ})$'s) close to a upright surface. The indeterminate situation, i.e., $m\Box 1/3$ (wedge), $m\Box 0.7$ (wedge),
corresponds to
$\square \square 90^{\circ}$'s and $\square \square 148^{\circ}$'s, respectively. The last situation consequently suggests a very sharp wedge shape.
Fig. 2a demonstrates that when m grows, the horizontal velocity rises and the width of the velocity boundary
layer falls. This is because increasing m results in the progression of velocity over the wall and hikes the
increase of the boundary layer. The vastness of the momentum is peak for values of $m\square$ 0and the optimal
velocity is obtained with $m \square 1.0$. Further the momentum is minimal for the Blasius flow $(m \square 0)$. Hence one
can conclude that steeper the wedge geometry higher the horizontal velocity. Again, an asymptotically
smooth profile is calculated in the free flow, which confirms the existence of a large enough infinite
boundary in the free flow. The similar observations were identified in reference [55] for the nanofluid
flowing past a wedge for a Newtonian fluid.
Fig. 2b illustrate the variation in secondary velocity $H(\Box)$ with m near the wedge surface as m increases the
angular velocity decreases suggesting that there microelements rotate progressively in the opposite direction.
Hence there is angular deceleration owing to the increasing reverse spin. This nature occurs in the range $0 \Box$
$\Box\Box$ 1 and for values of $\Box\Box$ 1, there is an acceleration in the angular velocity and sustained into the free
stream. Peak values of $H(\square)$ arise in the Blasius flow example ($m\square$ 0) and are progressively with growing
values of parameterm. For $m \square 1$, smooth increase in $H(\square)$ occurs from the boundary to the unrestricted flow.
However, for $m \square 1.0$ a specific monotonic increase occurs from the leading edge to the unrestricted flow.
For all values of m , the asymptotically smooth profiles converge at $\Box\Box$ 3.0 . The rotary movements of the
micro-elements are thus significantly influenced by the wedge parameter.
Fig. 2c shows the influence of m on temperature \square (). Increasing m clearly increases temperature, with the
biggest change occurring away from the wedge surface. Therefore, a bigger wedge parameter causes the
thickness of the thermal boundary layer to grow. In comparison to the Blasius flat plate example $(m \square 0)$, a
higher heating regime is created for the forward stagnation flow scenario ($m\Box 1.0$), with the wedge case
coming in between these two ends.
Fig. 2d displays the effect of m on \square \square (). Increasing m increases \square \square ()near the leading edge and the profiles
converge in the free stream for all values of m . The motile density boundary layer thickness therefore rises
with larger wedge parameter. The $\Box\Box$ () is maximum for $m\Box 1.0$ and minimal for $m\Box 0$. m arises in each term
of equation (16), as m is a function of \square^* and its effect is dominant in primary and angular momentum fields
rather than $\Box\Box$ (). The $\Box\Box$ ()attains the peak via forwarded stagnation scenario rather than any other

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geometrical case, although, (Fig. 4), heat sink (\square) has a considerably more significant impact and generates
a lot stronger cooling.
Fig. 3a – d elucidate the implication of material parameter (K) on the functions $F' \square \square \square$,
$H \square \square \square$, $\square \square \square \square$, and $\square \square$ () for $m \square 1/3$. A significant deceleration in primary flow (Fig.
3a) is caused, that is in contrast to the traditional responsiveness in the horizontal surface boundary layer
flow, as stated by Beg et al. [56], Gupta et al. [57] and Nath [58], amongst other. The normal impact of
micropolar fluids on reducing drag in horizontal plate flows cannot be realised in wedge flows because the
primary velocity is reduced. Furthermore, regardless of the Eringen parameter's value, no backflow is
produced, and primary velocity computations result in dependably smooth climbs from the wedge surface to
the liberate stream. Maximum acceleration is attained in the
Newtonian fluid scenario ($K \square 0$), and greatest deceleration is attained in the highly
dF^3
micropolar case ($K\square$ 2). Clearly, the revised shear term, i.e., $(1\square K)$ $d\square_3$ and the
dHcoupled factor, K , which features the Eringen Micropolar factor, generate
$d\Box$
significant changes in the primary velocity field. Therefore, the width of the border layer of the primary
velocity is augmented with Eringen micropolar vortex viscosity, i.e., higher values of K .
Fig. 3b shows that there is an increase in angular velocity near the wedge surface in the range of 0 \square \square 1.2
.However, quickly this pattern is reversed and there is a robust deceleration induced in angular momentum
with increasing vortex viscosity and then the profiles merge in the free stream. The rotary motions are
damped away from the wedge surface whereas they are boosted near the wedge surface. Fig. 3c promotes
the temperature field with increasing the vortex viscosity parameter K . The Newtonian fluid shows the
cooling effect in comparison with the Micropolar fluid. Fig. 3d also shows the similar effect on $\Box\Box$ () as that
of $\Box\Box$ () but the magnitude is different. The function $\Box\Box$ () is not much deteriorated with K .
Fig. 4 shows the progression of temperature with \Box , in the scenario of $m\Box 1/3$ (allinclusive wedge
movement). The wedge example above relates to a wedge angle of nearly 90° , i.e., a steep (perpendicular)
wedge geometry. For \square \square 1, monotonic declines into the free flow are seen, and the highest temperature is
calculated on the wedge surface (wall) in each profile. A kink develops in the zone close to the wall for the
case $\Box\Box$ 2.0, and a feeble climb thereafter takes place to the free flow. The removal of more thermal energy
from the boundary layer through the wall is implied by a stronger heat sink. As previously mentioned, this
method is employed in the production of polymers to avoid the additional heat build up caused by viscous
dissipation. As a result, manufactured items produce a more homogenous thermal diffusion and have a
stronger heat sink effect, which greatly reduces the temperature boundary layer width. Higher temperatures,
that are undesirable in processes involving the processing of materials, would undoubtedly ensue from the
absence of a heat $sink \square \square \square$ [59, 60]. In these flows, a heat source $\square \square \square \square \square$ is similarly unsuited for thermal
regulation; hence it is not taken into account in this context.
Fig. 5 shows how the viscous heating factors, $Ec\ u\ c\ T\Box\ ^2/\Box$ effect on temperature ($\Box\Box$ ()) changes.

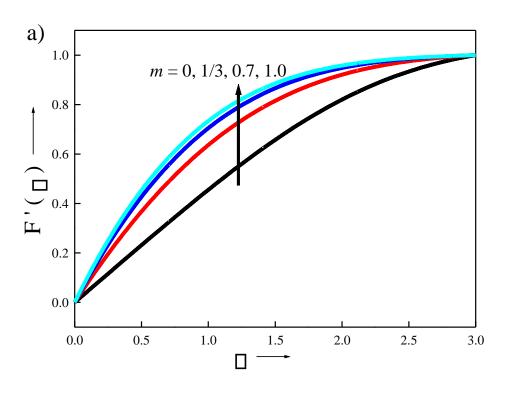
Viscous heating has a considerable impact on the flow of polymer coatings. As discovered by Winter [61], a

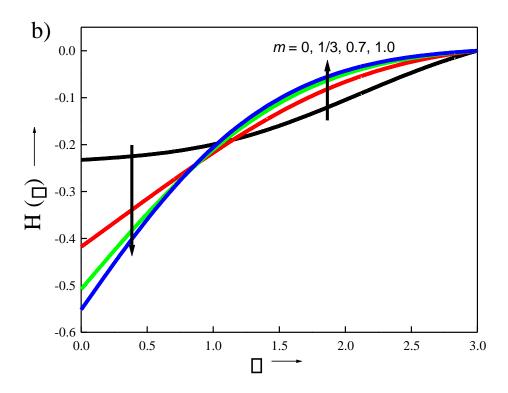
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part of the work of deformation is transformed into thermal energy by internal drag when a very sticky
liquid (such as polycarbonate mixture) is distorted in a fluid domain. The large value ($Pr \square 100$) is assigned
to the Prandtl number. Because of this, the thermal diffusivity in the flow is significantly higher than the
kinematic viscosity, and the heat conductance is likewise too much lower. In other words, heat is convicted
more slowly than momentum. According to the expression (1 \square K Ec F) \square " $^2\square G$ ' $^2\square$ in the temperature
border layer eqn.
15, this amplifies the contributions of the primary and secondary shear rates. When
$\mathit{Ec} \square 0$, viscous dissipation impacts are denied, and temperatures are reduced. The implication is that the
temperature field is under-predicted when viscous heating is ignored. Rising values of Ec (which correlates
the boundary layer enthalpy difference to the K. E. lost in the flows) leads to hike in the thermal boundary
layer thickness. Another thing to keep in mind is that the primary and secondary contributions to viscous
dissipation are both taken into account in the current research, but in the great part of research published in
the existing work, exclusively the primary momentum contribution is factored into models.
Fig. 6 depicts the effect of bioconvective Lewis number on motile microorganism density function ($\Box\Box$ ()).
At the wall, $\Box\Box$ () is large and equal for any value of Lb and falls down in the range $\Box\Box\Box\Box$ 0.6 . For $Lb\Box$
0.6all profiles converges and remains constant towards the free stream. Physically, for larger Lb values, the
diffusion coefficient of microorganisms' decreases and thus the locomotive denseness degrades.
The validation of the results have been carried out and depicted in table-1 with the published work [62, 63,
64]. This table shows that the current outcomes agree very well with the earlier published research. The
influence of m , K , I and Lb parameters on the wall primary stress, rotational momentum gradient, local heat
transport rate, and local density number of motile microorganisms is shown in table-2. The growth in the
value of m reveals the increasing impact on shear stress, couple stress, and local Nusselt number. For $m \square 1$,
i.e., in the forward stagnation point flow ($\Box\Box$ 1800s) the motile microorganism number drops but shows
increasing behavior for acute wedge. The motile microorganism number has dropped for $m\Box 1$, i.e. in the
forward stagnation point flow ($\Box\Box$ 180°), but improves for acute wedge angle. The impact of Kon the
couple stress, Nusselt and motile microorganisms' numbers diminishes, while the primary stress increases.
Further, an increase in micro-inertia parameter raises local Nusselt number and reduces both shear stress,
and couple stress but the local microorganisms number remains constant. The Lewis number of
bioconvection has no impact on F "(0) , H '(0) , and $\Box\Box$ "(0) . The increase in Lb shows an increasing effect
on the motile microorganisms' numbers.









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(d)

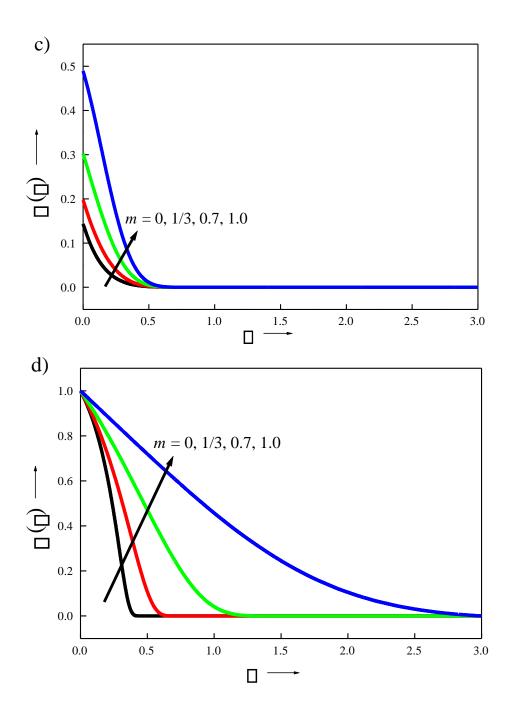
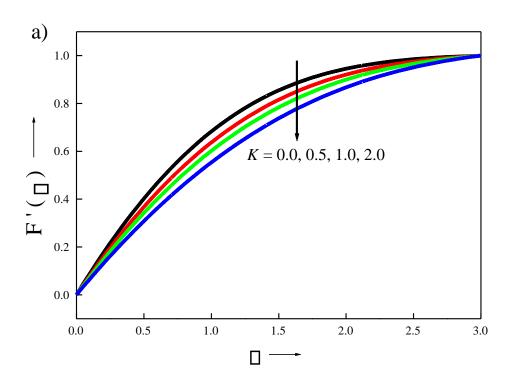
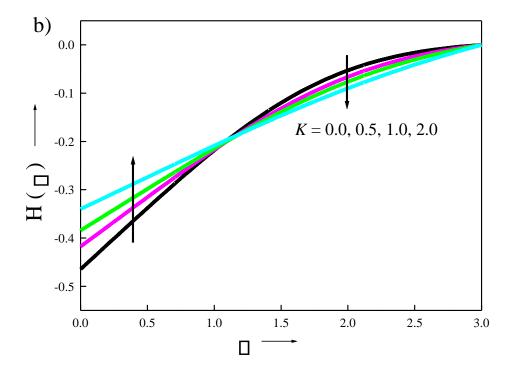


Figure 2. Profiles for **(a)** Primary velocity, **(b)** Angular velocity, **(c)** Temperature, Motile microorganism versus pressure gradient parameter.









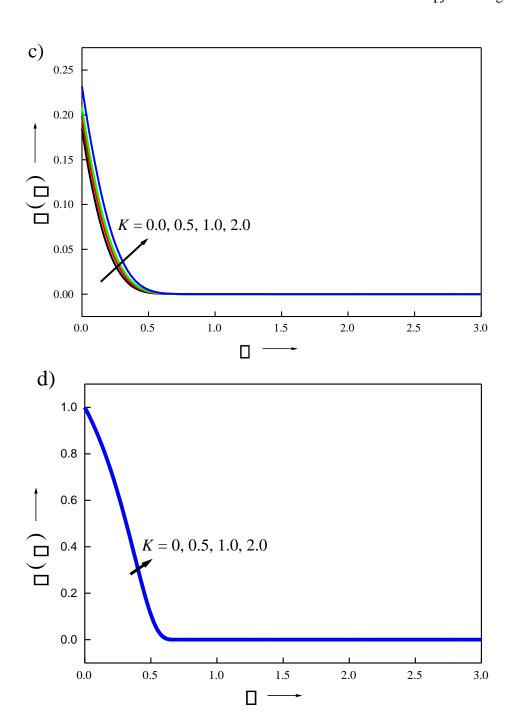


Figure 3. Profiles for **(a)** Primary velocity, **(b)** Angular velocity, **(c)** Temperature, and **(d)** Motile Microorganism versus vortex viscosity parameter.



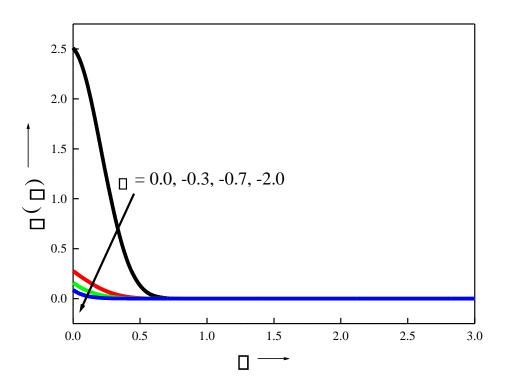


Figure 4.Profiles for temperature versus heat sink parameter.

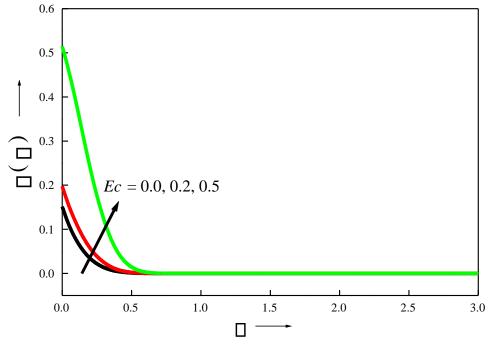


Figure 5. Profiles for temperature versus Eckert number.

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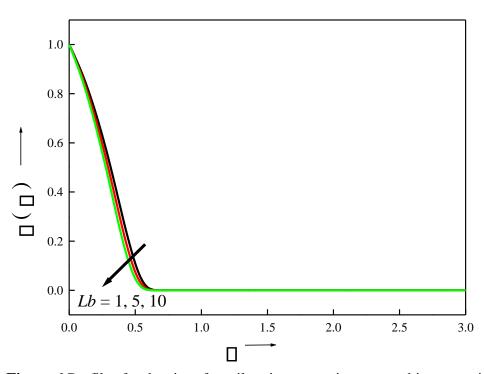


Figure 6.Profiles for density of motile micro-organism versus bioconvective Lewis number. **Table 1.** Values of wall shear stress (skin friction coefficient) when $K \square \square m = 0$ for $I \square 0.5$, $\square \square \square 0.5$, $Ec \square 0.2$, $Pr \square 100$.

K	m	Yih 62	Chamkha et al ⁶³	Ishak et al ⁶⁴	Present Result
0	0	0.332057	0.332206	0.332100	0.346600
0	1/3	0.757448	0.757586	0.757500	0.758600
0	1	1.232588	1.232710	1.232600	1.232815

Table 2. Values of F''(0), H'(0), $\square\square'(0)$, and $\square\square'(0)$, versus m, K, I and Lb.

m	K	I	Lb	C_{fx} Re	C_w Re	Nu	Mn
				<u>, </u>			R€
				2		R€	
0				0.4114	0.0089	4.9177	0.7972
1/3				0.8528	0.1366	4.1292	0.8665
1.0				1.3797	0.4016	2.0435	0.5640
	0			0.7586	0.1697	4.4246	0.8688
	0.5			0.8528	0.1366	4.1292	0.8665
	1.0			0.9415	0.1148	3.8972	0.8648



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	0		0.8536	0.1393	4.1271	0.8665
	0.1		0.8534	0.1386	4.1276	0.8665
	0.5		0.8528	0.1366	4.1292	0.8665
		1	0.8528	0.1366	4.1292	0.8665
		5	0.8528	0.1366	4.1292	0.9503
		10	0.8528	0.1366	4.1292	1.0402

Conclusion

Theoretical analysis of micropolar fluid flow across a wedge containing motile microorganisms has been introduced, including heat removal and sticky dissipation effects. Applying the MATLAB byp4c tool, a non-dimensional ODE boundary value problem was resolved using the 4th order RK-method. The important conclusions from the discussion that came before are as follows:

- 1. Primary velocity is augmented by the growing wedge parameter, whereas the vortex viscosity parameter shows the reverse effect.
- 2. Angular velocity is decreased near the wall versus m while it is increasing when $\Box \Box 1.0$. Further, Eringen viscosity parameter (K) shows the reverse effect.
- 3. Temperature is enhanced with increasing K values near the wedge surface in the region $0 \square \square 0.5$ and the temperature profiles converge to zero for $\square \square 0.55$ and remains constant towards the free stream.
- 4. The temperature and the width of the thermal boundary layer are significantly lowered by the effect of the rising wall heat sink, which cools the regime and aids in controlling the temperature in the dynamics of the polymer coating.
- 5. Increasing m increases $\Box\Box$ () at the leading edge, and the profiles come together in the free stream for all values of m.
- 6. Higher wedge parameter significantly lowers the Nusselt number, although the parameter *I* has little effect on it.
- 7. An enhancement in the values of bio-convection Lewis number improves M_n .
- 8. Primary drag force and rotational momentum gradient are both incremented with the growing m.
- 9. The wall couple stress, Nusselt and motile microorganism number are reduced with increasing Eringen viscosity parameter (K).

Nomenclature:

 $u \ v \ w$, : Translational velocity components. $x \ y \ z$, : Cartesian coordinates

c : Non-negative constant

 C_{fx} : Dimensionless primary skin-friction C_{fz} : Non-dimensional secondary skin-friction

 C_p : Specific heat

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C_w : Dimensionless wall couple stress c_w : Dimensional
wall couple stress
D_m : Diffusivity of microorganisms
Ec: Eckert number f : Body force per unit mass vector
F: Non-dimensional stream function F ': Primary velocity
G: Dimensionless secondary velocity
G : Angular velocity (micro-rotation) vector
H : Dimensionless angular velocity (microrotation)
I: non-dimensional micro-inertia density parameter j : Micro-inertia density
k: Thermal conductivity
K: Vortex viscosity parameter/material parameter l : Body couple per unit mass
vector
L : Arbitrary scale length
Lb: Bio-convection Lewis number m : Falkner-Skan
power law index M_n : Density number of microorganisms n
: Constant
N : Angular velocity in the $xy\square$ plane
Nu: Nusselt number
P: Thermodynamic pressure Pr : Prandtl number Q :
Heat sink parameter q_w : Surface heat flux q_n : Surface
motile microorganisms flux
Re: Reynolds number
T : Temperature function
T_w : Temperature at the wedge
T_{\square} : Temperature at free stream
U : External velocity
V : Translational velocity vector
Greek symbols
□□, : Spin gradient viscosity coefficients for micropolar fluids
□* : Hartree pressure gradient
☐ :Eringen spin gradient viscosity
☐ : Motile microorganisms function
☐ : Heat sink parameter (negative)
☐ : Similarity variable
☐ : Vortex viscosity coefficient
☐ :Eringen 2 nd order viscosity coefficient
□ : Newtonian dynamic viscosity



☐ : Kinematic viscosity

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New York, 1978.

and heat Transfer

from a

☐ : Dimensionless temperature
☐: Mass density of micropolar fluid
\square : Wedge angle
\Box_x : Primary dimensional wall shear stress
\square_w : Secondary dimensional wall shear stress
Subscripts w: Wall conditions
☐ : Ambient conditions Acknowledgements:
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